

IN THE CLAIMS

Please amend the claims as follows:

Claims 1-14 (Canceled):

Claim 15 (Currently Amended): A process ~~for preparing at least one olefin having from 8 to 12 carbon atoms from at least one olefin having from 4 to 6 carbon atoms~~ which comprises

- a) hydroformylating at least one starting olefin having from 4 to 6 carbon atoms to obtain at least one aldehyde product;
- b) hydrogenating the at least one aldehyde product to form at least one corresponding alcohol;
- c) dehydrating the at least one corresponding alcohol to produce at least one 1-olefin by elimination of water from the at least one corresponding alcohol; and
- d) obtaining at least one olefin having from 8 to 12 carbon atoms by metathesis reaction with elimination of ethylene from the at least one 1-olefin.

Claim 16 (Previously Presented): The process as claimed in claim 15, wherein said starting olefin is a mixture of olefins having from 4 to 6 carbon atoms, thereby producing a mixture of olefins having from 8 to 12 carbon atoms.

Claim 17 (Previously Presented): The process as claimed in claim 15, wherein the hydroformylating is conducted in the presence of a catalyst comprised of rhodium and a triorganophosphorus compound.

Claim 18 (Previously Presented): The process as claimed in claim 15, wherein the hydroformylating is conducted at a temperature ranging from 70 to 150° C.

Claim 19 (Previously Presented): The process as claimed in claim 15, wherein the hydrogenating is conducted in the presence of a catalyst of nickel, copper, copper/nickel, copper/chromium, copper/chromium/nickel, zinc/chromium or nickel/molybdenum.

Claim 20 (Previously Presented): The process as claimed in claim 15, wherein the hydrogenating is conducted under a gas phase total pressure 0.5 to 50 MPa.

Claim 21 (Previously Presented): The process as claimed in claim 15, wherein the hydrogenating is conducted at a temperature of 120 to 230° C.

Claim 22 (Previously Presented): The process as claimed in claim 15, wherein the dehydrating is conducted over a fixed-bed catalyst of an oxide of an alkaline earth metal, of aluminum, of indium, of gallium, of silicon, of scandium, of yttrium, of lanthanum, of titanium, of zirconium, of thorium or of a rare earth metal.

Claim 23 (Previously Presented): The process as claimed in claim 22, wherein the dehydrating is conducted over a fixed-bed catalyst of γ -aluminum oxide having a BET surface area 80 to 350 m²/g.

Claim 24 (Previously Presented): The process as claimed in claim 15, wherein the dehydrating is conducted at a temperature ranging from 200 to 500° C.

Claim 25 (Previously Presented): The process as claimed in claim 15, wherein the dehydrating is conducted continuously over a solid catalyst which consists formally of aluminum oxide and barium oxide.

Claim 26 (Previously Presented): The process as claimed in claim 15, wherein said metathesis reaction is conducted over a rhenium catalyst comprising Re_2O_7 on $\gamma\text{-Al}_2\text{O}_3$ or on mixed support material selected from the group consisting of $\text{SiO}_2/\text{Al}_2\text{O}_3$, $\text{B}_2\text{O}_3/\text{SiO}_2/\text{Al}_2\text{O}_3$ and $\text{Fe}_2\text{O}_3/\text{Al}_2\text{O}_3$.

Claim 27 (Previously Presented): The process as claimed in claim 16, wherein the starting olefin comprises isobutene and linear butenes.

Claim 28 (Previously Presented): The process as claimed in claim 16, wherein the starting olefin is a C_4 fraction selected from the group consisting of raffinate I, a selectively hydrogenated C_4 fraction from a cracker, C_4 fractions from FCC plants and C_4 -olefins prepared by the Fischer-Tropsch synthesis.

Claim 29 (Previously Presented): The process as claimed in claim 28, wherein said C_4 fraction is an industrial C_4 fraction having an isobutene content of greater than 3 % by weight.

Claim 30 (Previously Presented): The process as claimed in claim 27, wherein 3-methyl-1-butene is separated from the 1-olefin fraction comprising olefins having 5 carbon atoms which is obtained after the dehydrating.

Claim 31 (Previously Presented): The process as claimed in claim 27, further comprising adding a stream of the 1-olefin to said metathesis reaction, wherein the 1-olefin consists essentially of 1-pentene and 2-methyl-1-butene in a ratio of from 1000:1 to 10000:1.

Claim 32 (New): The process as claimed in claim 15, wherein said metathesis reaction is conducted at a temperature ranging from 20 to 200° C.

Claim 33 (New): The process as claimed in claim 26, wherein said metathesis reaction is conducted at a temperature ranging from 50 to 100° C.

Claim 34 (New): The process as claimed in claim 28, wherein said C₄ fraction is an industrial C₄ fraction having an isobutene content of greater than 10 % by weight.